

Sun Yu et al (USP 6,176,971) may not be applied to support an obviousness rejection because it is commonly owned with the present application. Under 35 U.S.C. §103(c), a patent applied as a 102(e) reference may not be applied to support an obviousness rejection if the patent is commonly owned with the application. Sun Yu et al and the present application are both owned by Andritz-Ahlstrom, Inc. Accordingly, the obviousness rejection of claims 21, 22 and 24 should be withdrawn and these claims allowed.

Further, these claims have been rewritten into independent form. The limitations of former independent claim 13 are included in amended claims 21, 22 and 24. Moreover, the claim 13 limitations have been revised to avoid the indefiniteness rejection of claim 13.

All claims are in condition for allowance. If any small matter remains outstanding, the Examiner is requested to telephone applicants' attorney. Prompt reconsideration and allowance is requested.

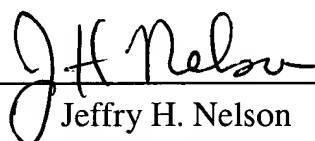
KETTUNEN et al
Serial No. 09/587,977

Attached hereto is a marked-up version of the changes made to the specification and claims by the current amendment. The attached pages are captioned "Version With Markings To Show Changes Made."

Respectfully submitted,

NIXON & VANDERHYE P.C.

By: _____


Jeffrey H. Nelson
Reg. No. 30,481

JHN:maw
1100 North Glebe Road, 8th Floor
Arlington, VA 22201-4714
Telephone: (703) 816-4000 ✓
Facsimile: (703) 816-4100

VERSION WITH MARKINGS TO SHOW CHANGES MADE

IN THE CLAIMS

Amend claims 21, 22 and 24 as follows

21. (Amended) A method [as in claim 13] of treating a first gaseous stream having a first pressure in a pulp mill to produce a second gaseous stream at a second pressure, higher than the first pressure, using a jet ejector having a high-pressure inlet, a low-pressure inlet, and a discharge outlet, said method comprising:

(a) introducing the first gaseous stream in the pulp mill having a first pressure to the low-pressure inlet of the jet ejector;

(b) introducing a second gaseous stream in the pulp mill to the high-pressure inlet of the jet ejector wherein the second gaseous stream is steam from a flash tank having hot spent cooking liquor from a cellulose pulp digester; and

(c) discharging a mixture of the two gaseous streams to form a third gaseous stream which is discharged from the discharge outlet at a third pressure, greater than the second pressure.

22. (Amended) A method [as in claim 13] of treating a first gaseous stream having a first pressure in a pulp mill to produce a second gaseous stream at a second pressure, higher than the first pressure, using a jet ejector having a high-pressure inlet, a low-pressure inlet, and a discharge outlet, said method comprising:

(a) introducing the first gaseous stream in the pulp mill having a first pressure to the low-pressure inlet of the jet ejector;

(b) introducing a second gaseous stream in the pulp mill to the high-pressure inlet of the jet ejector wherein the second gaseous stream is steam from a flash tank having hot spent cooking liquor from a kraft pulping process; and

(c) discharging a mixture of the two gaseous streams to form a third gaseous stream which is discharged from the discharge outlet at a third pressure, greater than the second pressure.

24. (Amended) A method [as in claim 21] of treating a first gaseous stream having a first pressure in a pulp mill to produce a second gaseous stream at a second pressure, higher than the first pressure, using a jet ejector having a high-pressure inlet, a low-pressure inlet, and a discharge outlet, said method comprising:

(a) introducing the first gaseous stream in the pulp mill having a first pressure to the low-pressure inlet of the jet ejector;

(b) introducing a second gaseous stream in the pulp mill to the high-pressure inlet of the jet ejector; and

(c) discharging a mixture of the two gaseous streams to form a third gaseous stream which is discharged from the discharge outlet at a third pressure, greater than the second pressure;

wherein the second gaseous stream is steam from a flash tank having hot spent cooking liquor from a cellulose pulp digester; and

wherein steps (a)-(c) are practiced so that a volume of the second gaseous stream is at least about 10% greater than would be discharged as steam from the flash tank without the utilization of the ejector under otherwise substantially identical conditions.